

# Chemical Reaction Engineering I

## Self Test 2

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# QUESTION 1

(a) The following liquid phase reaction



has the reaction kinetics (initial concentration of A is  $0.05 \text{ mol dm}^{-3}$ ), shown in Table 2

$C_A (\text{mol dm}^{-3})$	0.05	0.04	0.03	0.02	0.01
$-r_A (\text{mol dm}^{-3} \text{ s}^{-1})$	0.005	0.0042	0.003	0.0025	0.00125

The same reaction now will be conducted in a  $1200 \text{ dm}^3$  CSTR with its exit connected in-series to a PFR with volume of  $600 \text{ dm}^3$ . The entering  $C_{A0}$  and  $C_{B0}$  to a CSTR are  $0.05 \text{ mol dm}^{-3}$  and  $1 \text{ mol dm}^{-3}$ , respectively. In addition, the entering total volumetric flowrate is  $100 \text{ dm}^3 \text{ s}^{-1}$ . The exit conversion from the PFR is 80%.

- (i) Develop the Levenspiel Plot associated with the given data (refers to the table)
- (ii) Determine the intermediate conversions that can be achieved.



# QUESTION 2

Pure gas A enters the reactor at 830 kPa, having a volumetric flow rate,  $v_0$  of 4 dm<sup>3</sup>/s at 450 K. Find the initial concentration of A,  $C_{A0}$  and the entering molar flow rate,  $F_{A0}$ . Assume A is an ideal gas.



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