

# BIOREACTOR ENGINEERING Chapter 4 Operation Considerations for Bioreactor

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### **Chapter Description**

- Topic Outcome
  - Differentiate between batch and continuous modes of bioreactor operation
- References
  - Doran, P.M. (2013) Bioprocess Engineering Principles. Elsevier.
  - Liu, S. (2013) Bioprocess Engineering: Kinetics, Biosystem, Sustainability and Reactor Design. Elsevier.
  - Rao, D.G. (2010) Introduction to Biochemical Engineering. McGraw Hill.



### **Topic Outline**

• Choosing Cultivation Method



- Batch mode
- Continuous mode

Which type is more efficient?

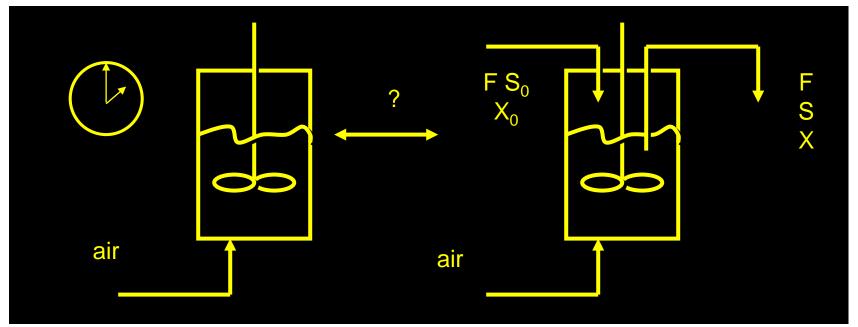
Which type is more common?



• Exercise 1



- PRODUCTIVITY: rate of product per time per volume.
  - Consider production of cell mass OR growth associated product in suspension culture





### **Batch mode**

Batch cycle time is:  $t_{cycle} = t_b + t_{dn}$ 

 $t_h$  = the time required for batch cell conversion  $t_{dn}$  = the downtime = preparation + lag time + harvest time

- So,  $t_{cycle} = \frac{1}{\mu_{\text{max}}} \ln \frac{X_f}{X_i} + t_{dn}$
- Cell production rate in one batch cycle is:  $(P_X)_{batch} = \frac{X_f X_i}{t_{cools}}$

$$(P_X)_{batch} = \frac{X_f - X_i}{t_{cycle}}$$

• Recall: 
$$Y_{X/S} = \frac{X_f - X_i}{S_i - S_f} = \frac{X_f - X_i}{S_i - 0}$$

• SO, 
$$(P_X)_{batch} = \frac{Y_{X/S}S_i}{\frac{1}{\mu_{\text{max}}} \ln \frac{X_f}{X_i} + t_{dn}}$$



### Continuous mode

• Recall: 
$$X = Y_{X/S} \left( S_0 - \frac{K_S D}{\mu_{\text{max}} - D} \right)$$
  $D_{opt} = \mu_{\text{max}} \left( 1 - \sqrt{\frac{K_S}{K_S + S_0}} \right)$ 

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- X at the maximum production rate:
- Productivity,  $P_x = DX$  when  $D = D_{opt}$  and X = X (at  $D_{opt}$ )

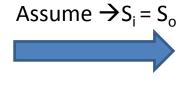
• SO, 
$$(P_X)_{\text{opt,cont}} = Y_{X/S} \mu_{\text{max}} \left[ 1 - \sqrt{\frac{K_S}{K_S + S_0}} \right] \left[ S_0 + K_S - \sqrt{K_S (S_0 + K_S)} \right]$$

- when  $S_0 >> K_s$
- So,  $(P_X)_{opt,cont} \approx \mu_{max} Y_{X/S} S_0$



Comparing the batch production rate and continuous production rate:

$$(P_X)_{batch} = \frac{Y_{X/S}S_i}{\frac{1}{\mu_{\text{max}}} \ln \frac{X_f}{X_i} + t_{dn}}$$



$$(P_{X})_{batch} = \frac{Y_{X/S}S_{i}}{\frac{1}{\mu_{\max}}\ln\frac{X_{f}}{X_{i}} + t_{dn}}$$
Assume  $\Rightarrow$  S<sub>i</sub> = S<sub>o</sub>

$$\frac{(P_{X})_{opt,cont}}{(P_{X})_{batch}} = \ln\frac{X_{f}}{X_{i}} + \mu_{\max}t_{dn}$$

$$(P_X)_{opt,cont} \approx \mu_{\max} Y_{X/S} S_0$$

- In general, X<sub>f</sub> >> X<sub>o</sub>, thus, continuous culture is better!
- Example: *E. coli* growing on glucose:

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$$X_f/X_o = 20$$
,  $\mu_{max} = 1 \text{ h}^{-1}$ ,  $t_{dn} = 5 \text{ h}$ ,  $\frac{(P_x)_{opt,cont}}{(P_x)_{batch}} = ?$ 

 Even so, most industrial fermentation processes occur in a batch reactor. Why?



### Batch mode is more common because:

- Productivity → Many industrial applications are for nongrowth associated products.
- Genetic stability → Continuous culture is detrimental to genetically engineered organisms. This makes continuous culture less productive.
- Operability and sterility → Long term continuous culture can be problematic.
- Market Economics → Batch system is flexible, able to make more than one product with the same reactor.



### Continuous mode is more efficient because:

- Higher productivity for cell and growth associated products because it offers a continuation of growth for a long period.
- It provides constant environmental conditions for growth and product formation.





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