

# SEPARATION PROCESS

## DRYING Part 2

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# Humidity

- Humidification - transfer of water from the liquid phase into a gaseous mixture of air and water vapor.
- Dehumidification - reverse transfer where the water vapor is transferred from the vapor state to the liquid state.
- **Humidity,  $H$**  – the kg of water vapor contained in 1 kg of dry air.

$$H = \frac{18.02}{28.97} \frac{p_A}{P - p_A}$$

- Saturated air is air in which the water vapor is in equilibrium with liquid water at given T and P. In this mixture the partial pressure of the water vapor is equal to the vapor pressure  $p_{AS}$  of pure water at given T

- **Saturation humidity,  $H_S$**  – 
$$H_S = \frac{18.02}{28.97} \frac{p_{AS}}{P - p_{AS}}$$

- **Percentage humidity,  $H_P$**  – 
$$H_P = 100 \frac{H}{H_S} = \frac{p_A}{p_{AS}} \frac{P - p_{AS}}{P - p_A} (100)$$

- **Percentage relative humidity,  $H_R$**  – 
$$H_R = 100 \frac{p_A}{p_{AS}}$$

# Humidity

- **Dew point** - the temperature at which a given mixture of air and water vapor would be saturated/ or temperature at which vapor begins to condense when the gas phase is cooled at constant pressure.
- **Humid heat,  $c_S$**  - amount of heat required to raise the temperature of 1 kg of dry air plus the watervapor present by 1 K.

$$c_S \text{ (kJ/kg dry air.K)} = 1.005 + 1.88H \text{ (SI)}$$

where,  $c_{P \text{ water}(v)} = 1.88 \text{ kJ/kg water vapor. K}$ ;  $c_{P \text{ air}} = 1.005 \text{ kJ/kg dry air. K}$

- **Humid volume,  $v_H$**  - total volume ( $\text{m}^3$ ) of 1 kg of dry air plus the vapor it contains at 1 atm abs pressure and the given gas temp.

$$v_H \text{ (m}^3\text{/kg dry air)} = (2.83 \times 10^{-3} + 4.56 \times 10^{-3} H) T \text{ (K)}.$$

- **Total enthalpy of an air-water mixture,  $H_Y$**  - the total enthalpy of 1 kg of air plus its water vapor/ or sensible heat of the air-water vapor mixture plus the latent heat if  $T_{ref}$  for both components = 0 °C

$$H_Y \text{ (kJ/kg dry air)} = (1.005 + 1.88 H) (T \text{ }^\circ\text{C} - T_{ref}) + \lambda_{ref} H$$

$$H_Y \text{ (kJ/kg dry air)} = (1.005 + 1.88 H) (T \text{ }^\circ\text{C} - 0) + 2501.4H$$

# Humidity Chart/Psychometrics Chart

Air entering a dryer has a dry bulb temperature of 60°C and a dew point of 26.7°C. Determine,  $H$ ,  $H_p$ ,  $c_s$  and  $v_H$

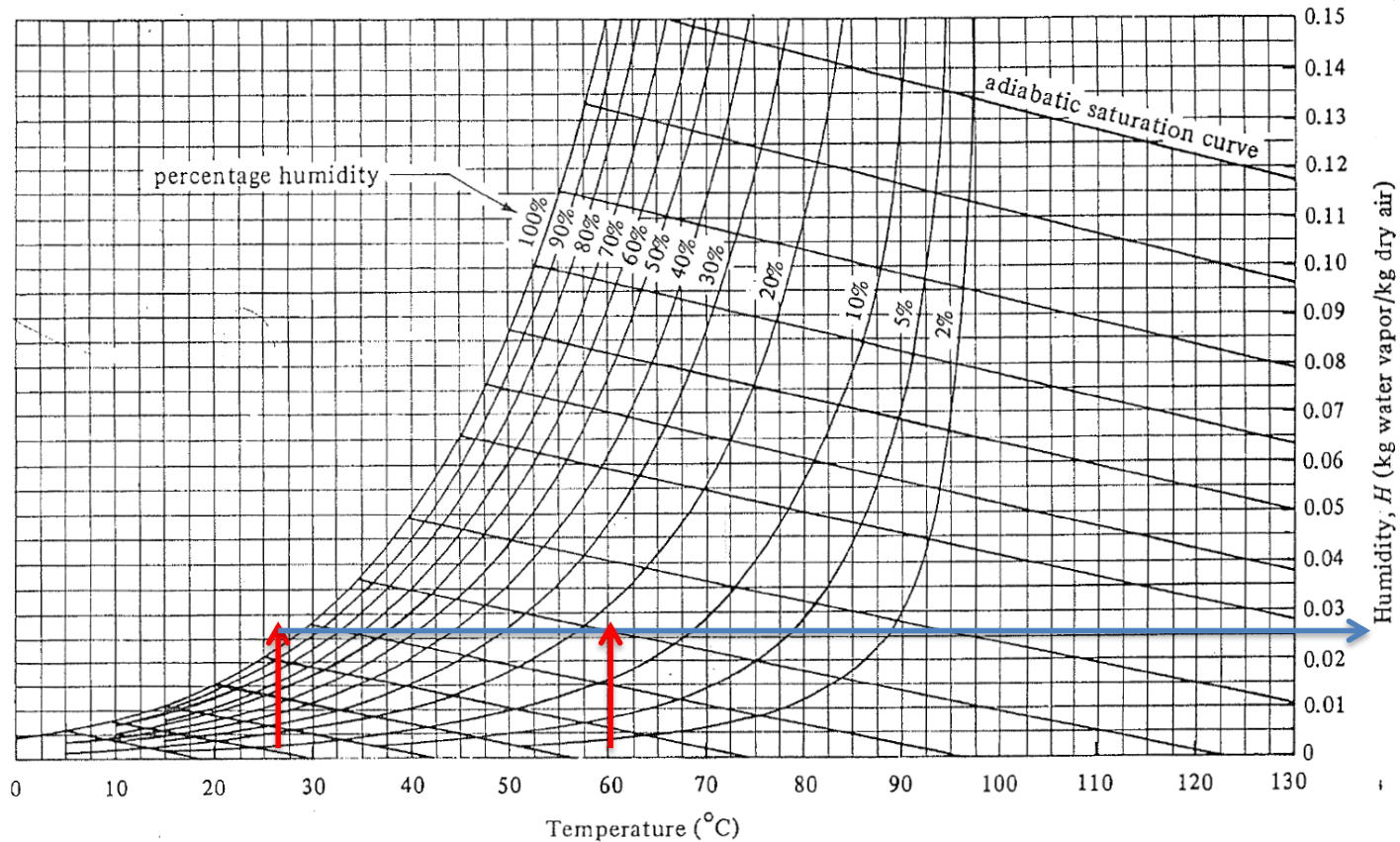


FIGURE 9.3-2. Humidity chart for mixtures of air and water vapor at a total pressure of 101.325 kPa (760 mm Hg). (From R. E. Treybal, *Mass-Transfer Operations*, 3rd ed. New York: McGraw-Hill Book Company, 1980. With permission.)

# Adiabatic Saturation Temperature, $T_s$

- The steady-state temperature attained when a large amounts of water is contacted with the entering gas.
- The leaving air is saturated at at  $T_s$  having a humidity  $H_s$ .
- Enthalpy balance ( $T_s$  is ref T)

enthalpy of the entering gas mixture = enthalpy of the leaving gas mixture.

$$c_s(T - T_s) + H\lambda_s = c_s(T_s - T_s) + H_s\lambda_s$$

$$\frac{H - H_s}{T - T_s} = \frac{c_s}{\lambda_s} = \frac{1.005 + 1.88H}{\lambda_s}$$

- If a gas mixture at  $T_1$  and  $H_1$  is contact for sufficiently long time in adiabatic contactor, it will leaves saturated at  $T_{s1}$  and  $H_{s1}$ .
- The values of  $H_{s1}$  and  $T_{s1}$  are determined by following the adiabatic saturation line going through point  $T_1, H_1$  until it intersect the 100% saturation line.
- If contact is not sufficient, the leaving mixture will be at a percentage saturation less than 100% bit on the same line.

# Wet Bulb Temperature $T_w$

- Steady-state nonequilibrium temperature reached when a small amount of water is contacted under adiabatic conditions by a continuous stream of gas.
- The amount of liquid is small so the  $T$  and  $H$  of the gas is not changed
- Method to measure  $T_w$  – thermometer is covered by wet wick or cloth
- A steady state water is evaporating to the gas stream. The water and wick cooled to  $T_w$  and stay at this constant temperature.
- Latent heat of evaporation is balanced by the convective heat flowing from the gas stream at  $T$  to the wick temperature  $T_w$
- The below equation can be assumed quite similar with adiabatic saturation lines with reasonable accuracy
- Hence wet bulb determination is often used to measure the humidity of an air-water vapor mixture

$$\frac{H - H_w}{T - T_w} = - \frac{h / M_B k_y}{\lambda_w}$$

# Equilibrium Moisture Content Of Materials

- A definite moisture content attain when the wet solid is exposing to the large excess air of air having constant T and H.
- Expressed as kg of water per kg of moisture-free (bone-dry) solid or kg H<sub>2</sub>O/100 kg dry solid
- Depend on the direction from which the equilibrium is reached
- In drying, wet sample is allowed to dry by desorption
- If the material contains less moisture than it equilibrium value, it will adsorb water until reaches its equilibrium value.
- Depends upon the structure of the solid, the temp. of the gas, & the moisture content of the gas.
- Varies greatly with the type of material for given % relative humidity

# Equilibrium Moisture Content Of Materials

- Bound water
  - The WC at 100% relative humidity
- Unbound water
  - Excess WC than indicated WC at 100% relative humidity
  - Held primarily in the voids of the solid
- substances containing bound water is called hygroscopic materials
- Free moisture content
  - moisture above the equilibrium moisture content at given % relative humidity.
  - moisture that can be removed by drying



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