

# **ENVIRONMENTAL ENGINEERING**

## Chapter 4 : Waste Water Treatment (Part 2) Secondary Treatment

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### **Chapter Description**

- Topic
  - Secondary treatment
- Expected Outcomes
  - Classify the treatment processes involved in wastewater treatment
  - Interpret the concept in wastewater treatment which consists of primary, secondary, sludge and advance treatment
- References
  - Peavy, H.S., Rowe, D.R. and Tchobanoglous, G., Environmental Engineering, McGraw Hill, 1985.
  - Mackenze, I.D., Introduction to Environmental Engineering, 4th Edition, Davis A. Cornell, Mc Graw Hill, 2008.
  - Sawyer, C.N. Chemistry for Environmental Engineerin. 4th Edition, McGraw Hill, 1994.
  - Martin, T.A. and David, W.H. Fundamental of Environmental Engineering. 2003.
  - Environmental Quality Act 1974 (Subsidiary Legislation), International Law Book, Service June 2002.









2- Suspended Culture System

- Suspended culture reactors may be of three basic types:
  - a) Completely mixed without sludge recycle.
  - b) Completely mixed with sludge recycle.
  - c) Plug flow with sludge recycle.





3- Activated Sludge

- Activated sludge a suspended-culture system that have been used since the early 1900s.
- Settled sludge containing living, or active, microorganisms is returned to the reactor to increase the available biomass and speed up the reactions.
- Process is aerobic, oxygen being supplied by dissolution from entrained air.



### (a) Completely Mixed Reactors





At steady state,

• No change in biomass or food concentration with time

Biomass in + biomass growth = Biomass out (effluent + wasted sludge)

$$Q_0 X_0 + V \left(\frac{k_0 XS}{K_s + S}\right) = \left(Q_0 - Q_w\right) X_e + Q_w X_u$$



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Food in – Food consumed = Food out

$$Q_0 S_0 - V \frac{k_0 SX}{Y(K_s + S)} = (Q_0 - Q_w)S + Q_w S$$

• Where  $Q_0, Q_w$  = influent & waste sludge flow rate

- X<sub>0</sub>, X, X<sub>e</sub>, X<sub>u</sub> = biomass concentration in influent, reactor, effluent & clarifier under flow
- $S_0$ , S = soluble food concentration (influent, reactor)
- $S_0$ , S = soluble • V = volume
- $k_s, k_0, k_d, Y = \text{kinetic constant}$





• Ratio of total biomass in the reactor per biomass wasted per given time:

$$\frac{VX}{Q_w X_u} = \theta_c$$

• Mean cell residence time,  $\theta_c$ :

$$\frac{1}{\theta_c} = \frac{Y(S_0 - S)}{\theta X} - k_d$$

• Mixed liquor suspended solids (MLSS), X:

$$X = \frac{\theta_c Y(S_0 - S)}{\theta (1 + k_d \theta_c)}$$

- Shortening θ, increase the MLSS
- θ approaches the
  regeneration time for
  microorganisms, cells
  are washed out of the
  reactor before growth
  can occur
- X decreases and S approaches S<sub>o</sub>, no treatment is occurring



(b) Plug-Flow Reactors





 $r_s = \frac{k_0}{Y} \frac{S\overline{X}}{K_s + S}$ 

Where X = average biomass concentration in the reactor (mg/L)

Only applicable when  $\theta_c/\theta \ge 5$ 



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$$\frac{1}{\theta_c} = \frac{k_0(S_0 - S)}{(S_0 - S) + (1 - \alpha)(K_s \ln S_i / S)} - k_d$$

#### Where

 $\alpha$  = recycle factor, Q/Qr Si= concentration of substrate after mixing with recycled sludge, mg/L.

$$S_i = \frac{S_0 + \alpha S}{1 + \alpha}$$



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# (c) Design considerations

- Design variable
  - Volumetric loading rates,  $V_L$
  - Food to mass ratios, F/M
  - Mean cell residence time,  $\theta_c$
- Complete mixed reactors wide fluctuations of flow rate occur.
- Plug flow reactor produce more mature sludge + excellent settling char.







•  $V_L$  = mass of BOD in the influent / volume of the reactor, kg BOD/m<sup>3</sup>.d

$$F/M = \frac{Q(S_0 - S)}{VX}$$

• F/M is the mass of BOD removed / biomass in the reactor (MLSS), kg BOD/kg MLSS.d





# F/M parameter

- Low F/M (low rate of wasting)
  - Starved organisms
  - More complete degradation
  - Larger, more costly aeration tanks
  - More  $O_2$  required
  - Higher power costs (to supply  $O_2$ )
  - Less sludge to handle
- High F/M (high rate of wasting)
  - Organisms are saturated with food
  - Low treatment efficiency





(d) Aeration of activated sludge

- Air diffusers inject compressed air into the biological reactor.
- Mechanical aerators mechanical mixers to stir the contents violently enough to entrain and distribute air through the liquid.





4- Ponds & Lagoons

• Oxidation Ponds: an open, flow through a large basin

of controlled shape specially design and constructed to treat sewage and bio-degradable industrial waste by natural processes involving bacteria and algae.

- Oxygen is provided by diffusion from the air and photosynthesis.
- **Lagoons:** oxygen is provided by artificial aeration (*e.g.* mechanical aerators).





Ponds & Lagoon System biology

- Anaerobic zone at the bottom, anaerobic bacteria, produce organic acids & gases as soluble food for aerobic zone
- Aerobic zone biological solid produced settle to the bottom, providing food for anaerobic bacteria





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Source:https://upload.wikimedia.org/wikipedia/commons/a/a9/Benfleet\_Sew age\_Treatment\_Plant%2C\_Filter\_Bed\_-\_geograph.org.uk\_-\_1450096.jpg

# **1. Trickling filter –** randomly packed solid medium



#### (RBC) – rotating disks partially

#### submerged in wastewater



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5- Attached Culture System



2. Bio-tower – advent of modular

synthetic media of high porosity and

low weight enables a vertical

high



5- Attached Culture System

(a) Attached-culture system biology

- Solid medium
- Biofilm organisms attach to medium, grow into dense films.
- Food for organisms dissolved organics, suspended particles, colloids, oxygen.
- Films grow thicker, create anaerobic site, attachment mechanisms weakened, biofilm washed away from medium (sloughing).



(b) Trickling filters



- Rotating distribution arm sprays primary effluent over circular bed of rock or other coarse media.
- Air circulates in pores between rocks.
- 'Biofilm' develops on rocks and microorganisms degrade waste materials as they flow past.
- Organisms slough off in clumps when film gets too thick.



Source:https://upload.wikimedia.org/wikipedia/commons/thumb/e/e0/Trickle\_F ilter.svg/2000px-Trickle\_Filter.svg.png



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Trickling filters

- Not a true filtering or sieving process.
- Material only provides surface on which bacteria to grow.
- Can use plastic media:
  - Lighter can get deeper beds (up to 12 m).
  - Reduced space requirement.
  - Larger surface area for growth.
  - Greater void ratios (better air flow).
  - Less prone to plugging by accumulating slime.



Source:https://upload.wikimedia.org/wikipedia/commons/a/a9/Benfleet\_Sew age\_Treatment\_Plant%2C\_Filter\_Bed\_-\_geograph.org.uk\_-\_1450096.jpg



(c) Bio towers



- Essentially deep trickling filters
- Lightweight, flat polyvinyl chloride sheets together.
- Can overcome the head loss problem.
- Operated in similar to high-rate trickling filters.
- Advantages:
  - a) Porosity and nature of the packing eliminate plugging problems.
  - b) Increased ventilation minimize odor problems.
  - c) Economical housing.



(d) Rotating Biological Contactors



- Called RBCs
- Consists of series of closely spaced discs mounted on a horizontal shaft and rotated while  $\sim 40\%$  of each disc is submerged in wastewater.
- Discs : light weight plastic.
- Slime is 1-3 mm in thickness on disc.



Source:https://upload.wikimedia.org/wikipedia/commons/3/3c/Rotating\_Biological\_Contactor.png



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6- Secondary clarification



- Activated sludge and attached-culture systems, solids are removed in secondary clarifiers.
- Ponds and lagoons, removal accomplished by settling within the reactor
- Design of secondary clarifiers for attached-culture systems similar to that for primary clarifiers



Source:https://upload.wikimedia.org/wikipedia/commons/1/1 8/Siloam\_Springs\_WWTP\_003.jpg



Activated-sludge clarifiers



- Two objectives:
  - Must produce an effluent
     sufficiently clarified to meet
     discharge standards.
  - Must concentrate the
    biological solids to minimize
    the quantity of sludge that
    must be handled.



Figure 10.26 Final clarifier for an activated-sludge secondary with rapid-sludge-removal apparatus. (Courtesv of Dorr-Oliver. Inc.)





# To be continued....



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